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Article II, Section 1 of the University of Idaho Student Code of Conduct states,

Cheating on classroom or outside assignments, examinations, or tests is a violation of this code. Plagiarism, falsification of academic records, and the acquisition or use of test materials without faculty authorization are considered forms of academic dishonesty and, as such, are violations of this code. Because academic honesty and integrity are core values at a university, the faculty finds that even one incident of academic dishonesty seriously and critically endangers the essential operation of the university and may merit expulsion.

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I have read and understand the above statement.

Signature

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## **EXAM INSTRUCTIONS – PLEASE READ THIS CAREFULLY**

You will have 50 minutes to complete this exam. This time limit will be strictly enforced. This is a CLOSED TEXTBOOK exam. The only resources allowed are a hand-held calculator and the course textbook supplement cited below,

Balmer, R.T., "Thermodynamic Tables to Accompany Modern Engineering Thermodynamics, Elsevier Inc., Burlington, MA, 2011.

You may use the blank pages in the booklet to write anything you desire IN YOUR OWN HANDWRITING. Absolutely no cutting and pasting in the book is allowed.

No computers, cell phones, iPhones, iPods, iPads, music players, or any other electronic equipment may be used during the exam with the exception of a hand-held calculator.

Show all of your work in the space provided on the exam. Partial credit cannot be awarded if the work is not shown. There are a total of 80 points on this exam—4 points per problem.



Date

## **CONVERSION FACTORS**

#### Length

$$\begin{split} 1 &m = 3.2808 \, ft = 39.37 \, in = 10^2 \, cm = 10^{10} \, \text{\AA} \\ 1 &cm = 0.0328 \, ft = 0.394 \, in = 10^{-2} \, m = 10^8 \, \text{\AA} \\ 1 &mm = 10^{-3} \, m = 10^{-1} \, cm \\ 1 &km = 1000 \, m = 0.6215 \, miles = 3281 \, ft \\ 1 &in = 2.540 \, cm = 0.0254 \, m \\ 1 &ft = 12 \, in = 0.3048 \, m \\ 1 &mile = 5280 \, ft = 1609.36 \, m = 1.609 \, km \end{split}$$

#### Energy

$$\begin{split} 1 &J = 1 \, N \cdot m = 1 \, kg \cdot m^2 / s^2 = 9.479 \, \times 10^{-4} \, Btu \\ 1 \, kJ = 1000 \, J = 0.9479 \, Btu = 238.9 \, cal \\ 1 \, Btu = 1055.0 \, J = 1.055 \, kJ = 778.16 \, ft \cdot lbf = 252 \, cal \\ 1 \, cal = 4.186 \, J = 3.968 \, \times 10^{-3} \, Btu \\ 1 \, Cal \, (in \, food \, value) = 1 \, kcal = 4186 \, J = 3.968 \, Btu \\ 1 \, erg = 1 \, dyne \cdot cm = 1 \, g \cdot cm^2 / s^2 = 10^{-7} \, J \\ 1 \, eV = 1.602 \, \times 10^{-19} \, J \end{split}$$

### Area

 $1 m^{2} = 10^{4} cm^{2} = 10.76 \text{ ft}^{2} = 1550 \text{ in}^{2}$   $1 \text{ ft}^{2} = 144 \text{ in}^{2} = 0.0929 \text{ m}^{2} = 929.05 \text{ cm}^{2}$   $1 \text{ cm}^{2} = 10^{-4} \text{ m}^{2} = 1.0764 \times 10^{-3} \text{ ft}^{2} = 0.155 \text{ in}^{2}$   $1 \text{ in}^{2} = 6.944 \times 10^{-3} \text{ ft}^{2} = 6.4516 \times 10^{-4} \text{ m}^{2} = 6.4516 \text{ cm}^{2}$ 

#### Volume

$$\begin{split} 1\,m^3 &= 35.313\,ft^3 = 6.1023 \times 10^4\,in^3 = 1000\,L = 264.171\,gal \\ 1\,L &= 10^{-3}m^3 = 0.0353\,ft^3 = 61.03\,in^3 = 0.2642\,gal \\ 1\,gal &= 231\,in^3 = 0.13368\,ft^3 = 3.785 \times 10^{-3}\,m^3 \\ 1\,ft^3 &= 1728\,in^3 = 28.3168\,L = 0.02832\,m^3 = 7.4805\,gal \\ 1\,in^3 &= 16.387\,cm^3 = 1.6387 \times 10^{-5}\,m^3 = 4.329 \times 10^{-3}\,gal \end{split}$$

#### Mass

 $\label{eq:states} \begin{array}{l} 1 \ \text{kg} = 1000 \ \text{g} = 2.2046 \ \text{lbm} = 0.0685 \ \text{slug} \\ 1 \ \text{lbm} = 453.6 \ \text{g} = 0.4536 \ \text{kg} = 3.108 \ \times 10^{-2} \ \text{slug} \\ 1 \ \text{slug} = 32.174 \ \text{lbm} = 1.459 \ \times 10^4 \ \text{g} = 14.594 \ \text{kg} \\ \end{array}$ 

1 N = 10<sup>5</sup> dyne = 1 kg·m/s<sup>2</sup> = 0.225 lbf

1 lbf = 4,448 N = 32,174 poundals

1 poundal = 0.138 N = 3.108 × 10<sup>-2</sup> lbf

#### Power

Density

$$\begin{split} 1 \ W &= 1 \ J/s = 1 \ kg \cdot m^2/s^3 = 3.412 \ Btu/h = 1.3405 \times 10^{-3} \ hp \\ 1 \ kW &= 1000 \ W = 3412 \ Btu/h = 737.3 \ ft \cdot lbf/s = 1.3405 \ hp \\ 1 \ Btu/h &= 0.293 \ W = 0.2161 \ ft \cdot lbf/s = 3.9293 \times 10^{-4} \ hp \\ 1 \ hp &= 550 \ ft \cdot lbf/s = 33000 \ ft \cdot lbf/min = 2545 \ Btu/h = 746 \ W \\ \hline \textbf{Pressure} \\ 1 \ Pa &= 1 \ N/m^2 = 1 \ kg/(m \cdot s^2) = 1.4504 \ \times 10^{-4} \ lbf/m^2 \end{split}$$

1 lbf/in<sup>2</sup> = 6894.76 Pa = 0.068 atm = 2.036 in Hg 1 atm = 14.696 lbf/in<sup>2</sup> = 1.01325  $\times$  10<sup>5</sup> Pa = 101.325 kPa = 760 mm Hg 1 bar = 10<sup>5</sup> Pa = 0.987 atm = 14.504 lbf/in<sup>2</sup> 1 dyne/cm<sup>2</sup> = 0.1 Pa = 10<sup>-6</sup> bar = 145.04  $\times$  10<sup>-7</sup> lbf/in<sup>2</sup>

 $1 \text{ in Hg} = 3376.8 \text{ Pa} = 0.491 \text{ lbf/in}^2$  $1 \text{ in Hg} = 248.8 \text{ Pa} = 0.0361 \text{ lbf/in}^2$ 

## MISCELLANEOUS UNIT CONVERSIONS

#### Specific Heat Units

 $1 Btu/(lbm \cdot ^{\circ}F) = 1 Btu/(lbm \cdot R)$ 1 kJ/(kg·K) = 0.23884 Btu/(lbm·R) = 185.8 ft·lbf/(lbm·R) 1 Btu/(lbm·R) = 778.16 ft·lbf/(lbm·R) = 4.186 kJ/(kg·K) **Energy Density Units** 1 kJ/kg = 1000 m<sup>2</sup>/s<sup>2</sup> = 0.4299 Btu/lbm 1 Btu/lbm = 2.326 kJ/kg = 2326 m<sup>2</sup>/s<sup>2</sup> **Energy Flux**  $1 \text{ W/m}^2 = 0.317 \text{ Btu/(h-ft}^2)$ 1 Btu/(h-ft<sup>2</sup>) = 3.154 W/m<sup>2</sup> Heat Transfer Coefficient  $1 W/(m^2 \cdot K) = 0.1761 Btu/(h \cdot ft^2 \cdot R)$  $1 Btu/(h \cdot ft^2 \cdot R) = 5.679 W/(m^2 \cdot K)$ Thermal Conductivity  $1 W/(m \cdot K) = 0.5778 Btu/(h \cdot ft \cdot R)$ 1 Btu/(h-ft-R) = 1.731 W/(m-K) Temperature  $T(^{\circ}F) = \frac{9}{5}T(^{\circ}C) + 32 = T(R) - 459.67$  $T(^{\circ}C) = \frac{5}{9}[T(^{\circ}F) - 32] = T(K) - 273.15$  $T(R) = \frac{9}{5}T(K) = (1.8)T(K) = T(^{\circ}F) + 459.67$ 

 $T(K) = \frac{5}{9}T(R) = T(R)/1.8 = T(^{\circ}C) + 273.15$ 

$$\label{eq:second} \begin{split} & 1 \ \text{lbm}/\text{ft}^3 = 16.0187 \ \text{kg/m}^3 \\ & 1 \ \text{kg/m}^3 = 0.062427 \ \text{lbm}/\text{ft}^3 = 10^{-3} \ \text{g/cm}^3 \\ & 1 \ \text{g/cm}^3 = 1 \ \text{kg/L} = 62.4 \ \text{lbm}/\text{ft}^3 = 10^3 \ \text{kg/m}^3 \\ & \textbf{Viscosity} \\ & 1 \ \text{Pa} \cdot \text{s} = 1 \ \text{N} \cdot \text{s}/\text{m}^2 = 1 \ \text{kg/(m} \cdot \text{s}) = 10 \ \text{poise} \\ & 1 \ \text{poise} = 1 \ \text{dyne} \cdot \text{s}/\text{cm}^2 = 1 \ \text{g/(cm} \cdot \text{s}) = 0.1 \ \text{Pa} \cdot \text{s} \\ & 1 \ \text{poise} = 2.09 \times 10^{-3} \ \text{lbf} \cdot \text{s}/\text{ft}^2 = 6.72 \times 10^{-2} \ \text{lbm}/\text{(ft} \cdot \text{s}) \\ & 1 \ \text{centipoise} = 0.01 \ \text{poise} = 10^{-3} \ \text{Pa} \cdot \text{s} \\ & 1 \ \text{lbf} \cdot \text{s}/\text{ft}^2 = 1 \ \text{slug}/(\text{ft} \cdot \text{s}) = 47.9 \ \text{Pa} \cdot \text{s} = 479 \ \text{poise} \\ & 1 \ \text{stoke} = 1 \ \text{cm}^2/\text{s} = 10^{-4} \ \text{m}^2/\text{s} = 1.076 \times 10^{-3} \ \text{ft}^2/\text{s} \\ & 1 \ \text{centistoke} = 0.01 \ \text{stoke} = 10^{-6} \ \text{m}^2/\text{s} = 1.076 \times 10^{-5} \ \text{st}^2/\text{s} \\ & 1 \ \text{m}^2/\text{s} = 10^4 \ \text{stoke} = 10^6 \ \text{centistoke} = 10.76 \ \text{ft}^2/\text{s} \end{split}$$

### COMMON MOLAR MASSES: C=12; H=1; O=16; N=14

## NOTE: MULTIPLE CORRECT ANSWERS ARE POSSIBLE ON NON-QUANTITATIVE PROBLEMS. For PARTIAL CREDIT on <u>non-quantitative problems</u>, supply supporting reasoning as you feel necessary. For FULL CREDIT <u>quantitative problems</u>, document <u>ALL</u> equations, conversions, and tables used.

- 1. What is the correct definition of <u>quality</u> within the two phase region?
  - a) mass fraction of saturated liquid
  - b) mass fraction of saturated vapor
  - c) volume fraction of saturated liquid
  - d) volume fraction of saturated vapor
- 2. Which of the following statements are true about the entropy balance equation,  $S_T + S_p = S_g$ ?
  - a)  $S_{g}$  is the entropy gain of the system during a finite interval
  - b)  $S_{\text{T}}$  is a transport term that includes effects of only heat transfer and mass transfer
  - c) S<sub>g</sub> can be positive, negative, or zero depending on the process
  - d) S<sub>p</sub> is zero for reversible processes
- 3. Saturated liquid water is in thermodynamic equilibrium inside a cylinder covered with a massless, moveable piston subjected to an external pressure of 1 MPa. What is the temperature of this fluid?
  - a) 100 C
  - b) 140 C
  - c) 180 C
  - d) 220 C
- 4. If 1 kg of saturated liquid water at 1 MPa is <u>heated isobarically</u> until the quality is 0.5, how much heat is added?
  - a) +1008 kJ
  - b) +1296 kJ
  - c) +1390 kJ
  - d) +2015 kJ
- 5. What is the specific entropy of water at 1 MPa if has a quality of 0.5?
  - a) 2.1391 kJ/kg-K
  - b) 3.2937 kJ/kg-K
  - c) 4.3632 kJ/kg-K
  - d) 4.4482 kJ/kg-K
- 6. How many kgmol are in 1 kg of liquid water  $(H_2O)$ ?
  - a) .056 kgmol
  - b) .061 kgmol
  - c) .066 kgmol
  - d) .071 kgmol

- 7. What process condition(s) might you apply when modeling/analyzing a turbine?
  - a) aergonic
  - b) isenthalpic
  - c) adiabatic
  - d) isentropic
- 8. What process condition(s) might you apply when modeling/analyzing a valve?
  - a) aergonic
  - b) isenthalpic
  - c) adiabatic
  - d) isentropic
- 9. Which of the following are thermodynamic <u>state functions</u> (as opposed to path functions)? a) specific internal energy
  - b) specific entropy
  - c) specific enthalpy
  - d) specific heat transfer
- 10. What is the value of the <u>polytropic exponent</u> for <u>isentropic expansion</u> of air? (Assuming constant heat capacities. HINT: Use data from Table C.13a.)
  - a) 1.00
  - b) 1.33
  - c) 1.40
  - d) 1.67
- 11. An ideal gas must <u>always</u> satisfy which of the following relationships?
  - a) Cp-Cv = R
  - b) pv = mRT
  - c)  $p_1v_1/T_1 = p_2v_2/T_2$
  - d) dq = Tds
- 12. Air at 727 C and .8 MPa enters a gas turbine at 10 kg/s and exits at 327 C and .1 MPa. What is the power output of this device, assuming variable specific heats. HINT: Use the air tables.
  - a) 3240 kW
  - b) 4390 kW
  - c) 4410 kW
  - d) 6070 kW

- 13. If a fluid with a <u>specific volume</u> of 1.5 m<sup>3</sup>/kg flows at 3 kg/s through a 20 cm diameter pipe, what is its velocity?
  - a) 35 m/s
  - b) 57 m/s
  - c) 143 m/s
  - d) 173 m/s
- 14. In what thermodynamic state is water at 375 C and 25 MPa?
  - a) compressed liquid region
  - b)two phase region
  - c) superheated vapor region
  - d) supercritical region
- 15. Which of the following statements are true for a Carnot Heat Pump?
  - a) the coefficient of performance (COP) is independent on the working fluid selected
  - b) the COP has an upper limit of 100%
  - c) the COP increases as the temperature difference between the heat source and heat sink increases
  - d) the COP is greater than the COP for the same device operating as a refrigerator
- 16. What is the change in entropy of an ideal gas that is heated <u>isochorically</u> from 27 C to 327 C? For this gas,  $C_p = .280$  Btu/lbm-R and  $C_v=.130$  Btu/lbm-R.
  - a) .0901 Btu/lbm-R
  - b) .1941 Btu/lbm-R
  - c) .3243 Btu/lbm-R
  - d) .6984 Btu/lbm-R
- 17. What information can be extracted from a temperature-entropy diagram for a closed system?
  - a) heat transfer for any reversible thermodynamic process
  - b) net heat transfer for any reversible thermodynamic cycle
  - c) work transfer for any reversible thermodynamic process
  - d) net work transfer for any reversible thermodynamic cycle
- 18. What does the first law reduce to for filling a tank with <u>flexible</u>, <u>but insulated walls</u> that are exposed to atmosphere? Neglect kinetic and potential energy terms. State 1 is the entering stream. State 2 is after filling.
  - a) Q +  $m_2h_1 = m_2u_2$
  - b)  $-W + m_2h_1 = m_2u_2$
  - c)  $Q m_2 h_2 = m_2 u_2$
  - d) W  $m_2h_2 = m_2u_2$

Problems 19 and 20 apply to an oceanic thermal energy system that operates in a cyclic fashion between a high temperature at 80 F (at the surface) and a low temperature at 40 F (deep under water).

- 19. What is the maximum thermal efficiency of a heat engine operating between these reservoirs?
  - a) 5.5%
  - b) 7.5%
  - c) 16.5%
  - d) 50%
- 20. What is the <u>maximum power output</u> of this heat engine if 5 MW of thermal power flows from the high temperature source?
  - a) 370 kw
  - b) 530 kw
  - c) 750 kw
  - d) 1000 kw