

## Convection - External Flow Example Values

### Flat Plate

#### Average temperature of 300 K

- $c_p = 1007 \text{ [J/kg-K]}$
- $\mu = 184.6\text{E-}7 \text{ [N-s/m}^2\text{]}$
- $k = 26.3\text{E-}3 \text{ [W/m-K]}$
- $\rho = 1.1614 \text{ [kg/m}^3\text{]}$

#### Case 1:

- Free-stream velocity: 15 m/s
- Length of plate: 1.5 m

#### Calculated Values

- $L_{\text{critical}} = 0.53 \text{ m} \rightarrow$  use turbulent flow values
- Reynolds number at end of plate: 1.42 E6
- $h_{\text{bar}} = 47.63 \text{ W/m}^2\text{K}$

#### Case 2:

- Free-stream velocity: 5 m/s
- Length of plate: 0.25 m

#### Calculated Values

- $L_{\text{critical}} = 1.59 \text{ m} \rightarrow$  use laminar flow values
- Reynolds number at end of plate: 78,643
- $h_{\text{bar}} = 17.45 \text{ W/m}^2\text{K}$

#### Case 3:

- Free-stream velocity: 5.5 m/s
- Length of plate: 1.5 m

#### Calculated Values

- $L_{\text{critical}} = 1.45 \text{ m} \rightarrow$  Should check both values – too close to tell from equations along
- Reynolds number at end of plate: 519,044
- $h_{\text{bar\_laminar}} = 7.47 \text{ W/m}^2\text{K}$
- $h_{\text{bar\_turbulent}} = 21.35 \text{ W/m}^2\text{K}$

## Cylinder in Cross-Flow

### Average temperature of 300 K

- $c_p = 1007$  [J/kg-K]
- $\mu = 184.6E-7$  [N-s/m<sup>2</sup>]
- $k = 26.3E-3$  [W/m-K]
- $\rho = 1.1614$  [kg/m<sup>3</sup>]

### Case 1:

- Free-stream velocity: 10 m/s
- Diameter of cylinder: 0.0127 m

### Calculated Values

- $Re_D = 7,990 \rightarrow$  Look up values for C and n
- $C = 0.193$
- $n = 0.618$
- $h_{bar} = 91.9$  W/m<sup>2</sup>K

### Case 2:

- Free-stream velocity: 10 m/s
- Diameter of cylinder: 0.1 m

### Calculated Values

- $Re_D = 62,914 \rightarrow$  Look up values for C and n
- $C = 0.0266$
- $n = 0.805$
- $h_{bar} = 45.46$  W/m<sup>2</sup>K

### Case 3:

- Free-stream velocity: 5 m/s
- Diameter of cylinder: 0.00008 m (approximate human hair diameter)

### Calculated Values

- $Re_D = 25.17 \rightarrow$  Look up values for C and n
- $C = 0.911$
- $n = 0.385$
- $h_{bar} = 923.7$  W/m<sup>2</sup>K